



Study the Effect of SiO₂ Nanofluids on Heat Transfer in Double Pipe Heat Exchanger

NOOR SABEEH MAJEED¹, SHAYMAA MAHDI SALIH²,
HUSSAM NADUM ABDA LRAHEEMAL ANI³, BASMA ABBAS ABDULMAJEED⁴,
PAUL CONSTANTIN ALBU⁵, GHEORGHE NECHIFOR^{6*}

¹Chemical Industries Department, Institute of Technology-Baghdad, Middle Technical University, Baghdad, Iraq.

²Materiel Engineering Department, University of Technology, Baghdad, Iraq.

³Chemical Industries Department, Institute of Technology-Baghdad, Middle Technical University, Baghdad, Iraq.

⁴Chemical Engineering Department, University of Baghdad, Baghdad, Iraq

⁵IFIN Horia Hulubei, Radioisotopes & Radiat Metrol Dept DRMR, 30 Reactorului Str, Magurele, 023465, Romania

⁶Politehnica University of Bucharest, Department of Analytical Chemistry and Environmental Engineering, 1-7 Gheorghe Polizu Str., 011061, Bucharest, Romania

Abstract: In this paper the effect of nanofluid is studied in the double pipe heat exchanger counter current flow, the viscosity of nanofluids are measured at different temperatures and different particle sizes. SiO₂ nanoparticles are dispersed at different concentrations (0.2-2) % with different particle sizes of (50-25) nm in base fluid of water. The friction factor and heat transfer coefficient are calculated at different nanoparticle sizes, the results showed that the viscosity was increased as nanoparticle concentration increased. The friction factor is increased as SiO₂ nanoparticles concentration and increased as nanoparticles size decreased. The heat transfer coefficient increased as nanoparticle concentration increased and particles size decrease.

Keywords: nanofluids, heat exchanger, viscosity, friction factor

1.Introduction

Efficiency in transferring the heat and minimizing the heat waste represent main concerns in the industrial applications. Nanofluids are widely used to enhance the heat transfer rate. Nanofluids represent a suspension of the nanoparticles in certain base fluids. Considering their properties, they have different ones compared with the already known mixtures of solid-liquid combinations. The excellent chemical and physical properties of these mixtures made the nanofluids to be used in a wide application of heat transfer enhancing processes [1-3].

Usually the metal oxides of nanoparticles have better thermal properties than the base fluids [4-7]. Choi in 1995 used the nanoparticles for the first time [3, 8, 9]. Choi found that when adding solid particles with sizes less than 100 nm, the thermal conductivity of the nanofluids increased higher than the base fluid [3, 10].

Peñas *et al.* [11] were used the technique of hot-wire that used two types of nanoparticles SiO₂ and CuO in water and ethylene glycol to measure the thermal conductivity. They used different weight fraction up to 5%, the results showed that the thermal conductivity of nanofluids have good results. Namburuet *et al.* [12] were used another types of nanoparticles SiO₂ with different particle sizes (20, 50, 100) nm to calculate the viscosity and specific heat of nanofluid with ratio 60:40 water and ethylene glycol base fluid; giving a new correlation employing experimental data. Another research studies the effect of volume concentration and the temperature to measure the viscosity of TiO₂/water nanofluid. The range of temperature was between 25 to 70 °C with fraction of 0.1, 0.4, 0.7 and 1% as in [13]. A spiral coil of five turns made of copper tube which used to investigate the nanofluid of different volume fraction of (0.01, 0.025, and 0.05) %. The results showed that the Nusselt number increased compared to the base fluid water. The friction factor was also studied and the result showed

*email: doru.nechifor@yahoo.com

that the friction factor increased as nanoparticle concentration increased, Duangthongsuk, W. [14]. Vajjha R. *et al.* [15] calculate the pressure drop of circular tube for the three types of nanofluids (CuO, SiO₂, and Al₂O₃), the results showed that the heat transfer rate increased as nanoparticles concentration increased and the pressure increased as the volume fraction increased too. SiO₂ and Al₂O₃ nanoparticles dispersed in the base fluid water and the study the heat transfer rate at concentration of (0.5 to 2) % with particles in size of range from 10 to 100 nm as given by Minakov A. *et al.* [16]. Hamid K. *et al.* [17] studied the heat transfer coefficient and the friction factor of TiO₂ nanofluid. Zarringhalam M. *et al.* [18] studied the effect of pressure drop and the heat transfer coefficient of CuO nanofluid with water base fluid. The experimental data was collected from a double tube heat exchanger in turbulent flow region. The results showed that at 2% volume fraction the heat transfer coefficient increased by 57%. Yarmand H. *et al.* [19] used graphen nanoparticles in turbulent flow region of a rectangular pipe. The heat transfer coefficient and the friction factor increased 19.68% and 9.22% for 0.1% volume fraction. In this paper silicon oxide nanoparticles are used two range of particle sizes of (50 & 25) nm, synthesis in the base fluid water at different temperatures in double pipe heat exchanger under turbulent flow region, to study the effect of nanoparticles in viscosity, friction factor and heat transfer coefficient of SiO₂ nanofluids at different concentrations.

2. Materials and methods

2.1. Experimental setup

Double pipe heat exchanger made of stainless steel is used to study the effect of nanofluids on the friction factor in the heat exchanger. The nanofluids enter the outer pipe of 30 cm in diameter with a range of temperatures (15, 20, 25, and 30) °C. Steam at 120°C enters the inner pipe of diameter 15 cm. The pressure is measured by gage and the temperature of outer fluid is recorded by thermocouples which are fixed at the inlet and outlet of cold and hot streams. Figure (1) shows the heat exchanger used in this research.



Figure 1. The experimental work, general view of the installation

2.2. Preparation of nanofluids

Silicon dioxide nanoparticles are in the form of white powder from (M K Impex Crop., USA) with two particle sizes (50 and 25) nm. The SiO₂ nanoparticles are added to the water base fluid at different weight fraction (0.2-2) %. The nanofluids prepared by second method, nanoparticles are synthesized

into water by mixing with mixer at speed of 300 rpm. Then the nanofluids are stabilized by sonication (MTI Corporation made in USA) it for 20 min to enhance the stability of nanofluid prepared.

2.3. The expressions used

The expression Blasius H. [20] is used to calculate the coefficient of friction of the nanofluid with silicon dioxide of different weight fraction has the form (1), and for the Nusselt number the Dittus Boelter relation is used in the form (3):

$$f = 0.3164 \cdot Re^{-0.25}; \quad (1)$$

$$Re = \frac{\rho d u}{\mu}; \quad (2)$$

$$Nu = \frac{h}{k} d = 0.023 Re^{0.8} Pr^{0.4}. \quad (3)$$

3. Results and discussions

3.1. The effect of weight fraction of nanofluids

The viscosity of nanofluids is measured at different temperatures (15, 20, 25, 30) °C by viscometer (ASTM D445). The results showed that the viscosity increased as nanoparticle weight fraction increased. This is agreed with Ahmet B. D., 2019 [21] as shown in Figures below.

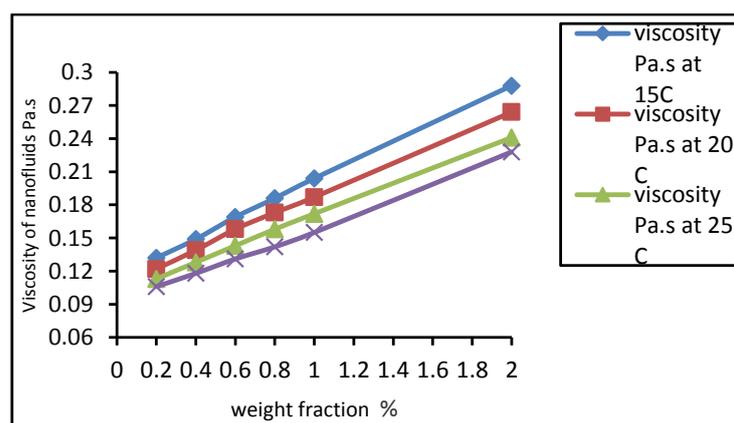


Figure 2. The viscosity of nanofluids at different temperatures

The friction factor of SiO₂ nanofluid increased as weigh fraction increased at different temperatures (15, 20, 25 and 30) °C as shown in Figures 3, 4, 5 and 6. This is agreed with Azmi W.H., 2017 [22].

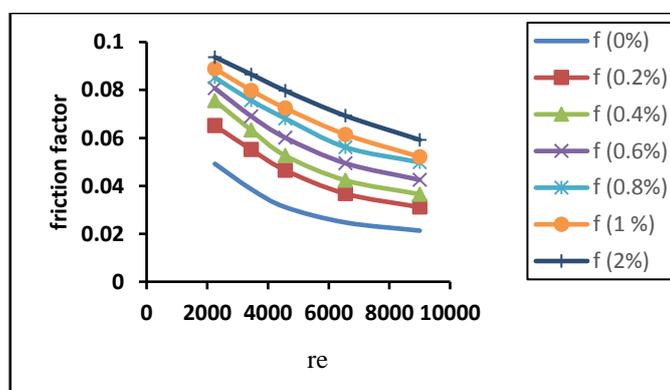


Figure 3. The friction factor at different weight fraction of SiO₂ at 15°C

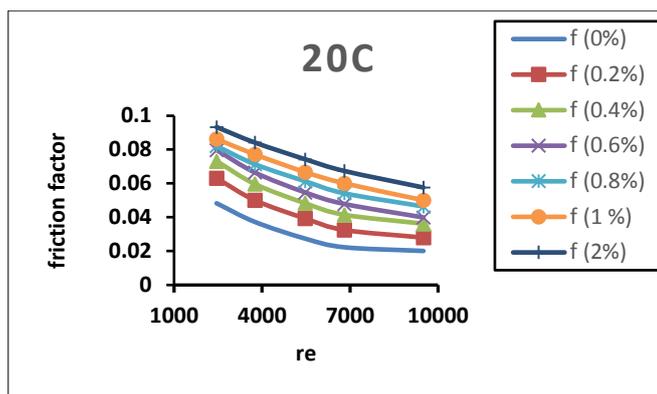


Figure 4. The friction factor at different weight fraction of SiO_2 at 20°C

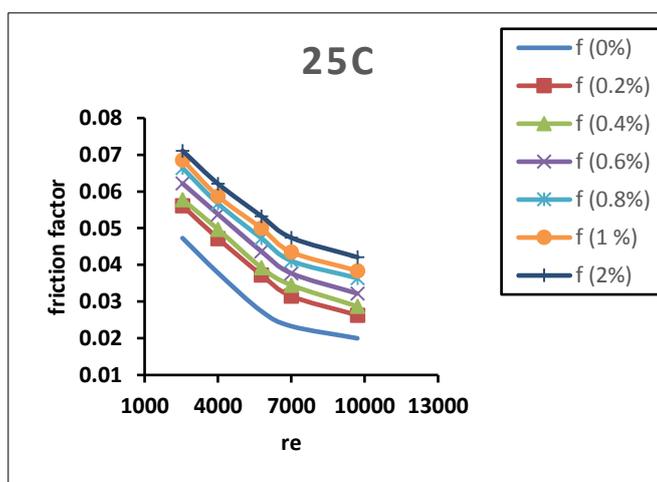


Figure 5. The friction factor at different weight fraction of $\text{SiO}_2/\text{water}$ at 25°C

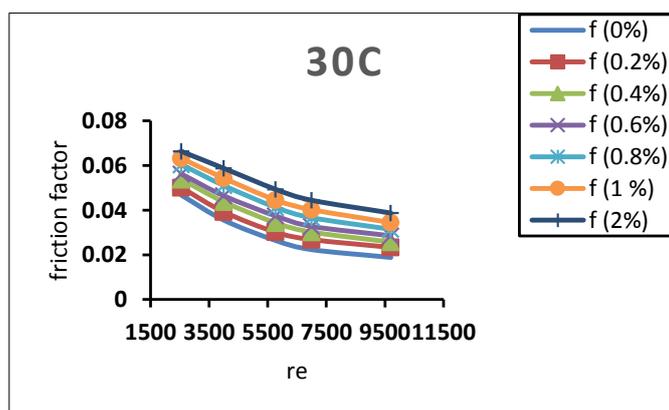


Figure 6. The friction factor at different weight fraction of SiO_2 at 30°C

The heat transfer coefficient of $\text{SiO}_2/\text{water}$ increased as nanoparticle weight fraction increased for different inlet temperatures as shown in Figure 7. The results are agreed with Devdatta P. and [23, 24].

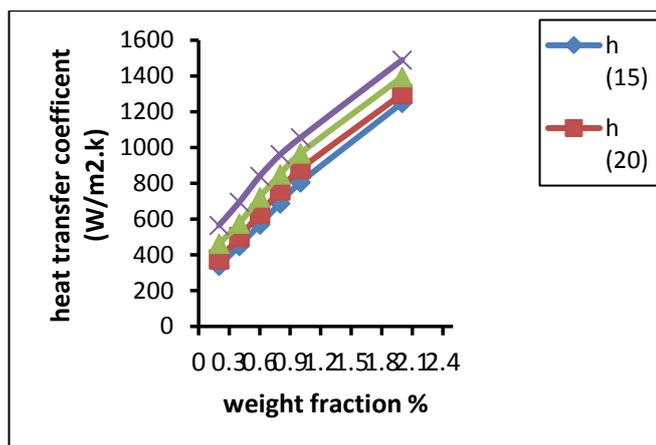


Figure 7. Heat transfer coefficient of SiO₂/water nanofluids at different temperatures

3.2. The effect of particle size of nanoparticles

The friction of SiO₂ nanofluids with (50 and 25) nm particle size are calculated. The friction of SiO₂/water of 50 nm had lower value in friction factor compared to SiO₂/water of 25 nm particle size. Figure 8 shows the friction factor of two particle size at 25 °C temperature degree. This is agreed with Suad H. D., 2018 [25].

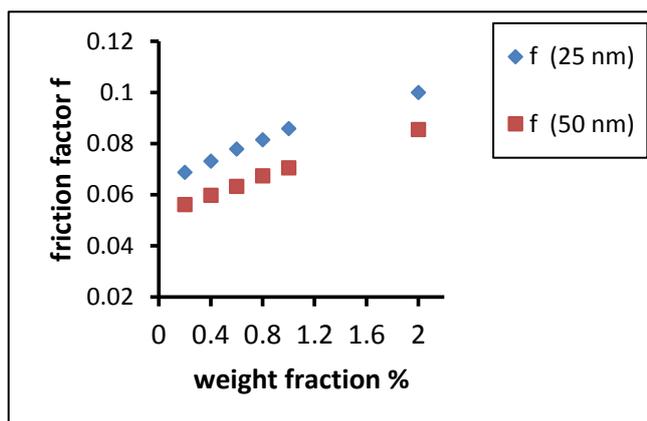


Figure 8. Friction factor of SiO₂/water nanofluid at two particle sizes (25 and 50) nm

The size of nanoparticles particles influences the value of heat transfer coefficient; the particle size of 25 nm SiO₂ has a higher heat transfer value than the particle size of 50 nm, of the same concentration. Figure 9 shows the heat transfer coefficient of 2% concentration at 25 °C temperature degree. This is agreed with Vivekanand L. K., 2017 [25].

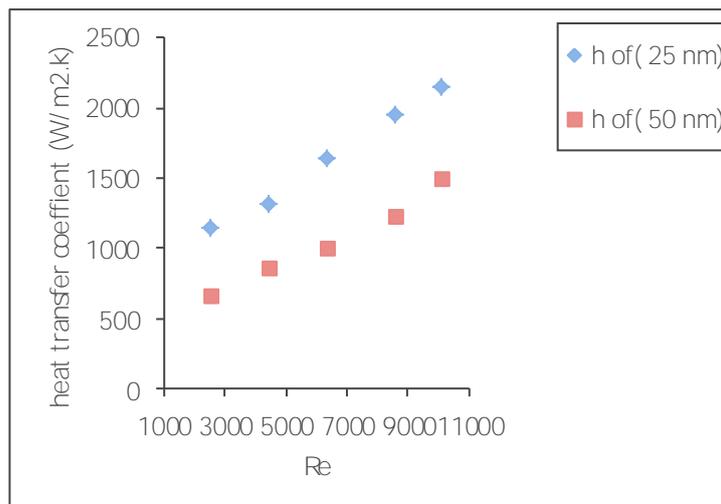


Figure 9. Heat transfer coefficient SiO₂/water nanofluid of two particle size (25 and 50) nm at 2% concentration and 25°C

4. Conclusions

The viscosity of SiO₂/water nanofluids increased as weight fraction increased, this is because of the distribution of SiO₂ nanoparticles in the base fluid water. The viscosity SiO₂/water nanofluid decrease as temperature of inlet fluid.

The friction factor increased as nanoparticle concentration increased because of the increasing in viscosity for different inlet temperature. The friction factor increased by 42% to the base fluid water at weight fraction 2% and 30°C.

The heat transfer coefficient increased as the concentration of SiO₂/water nanofluids with different temperature. This increment by 75% for 2% weight fraction and 30°C.

The friction factor of 25 nm particle size has high value of friction than the 50 nm. This is due agglomeration of nanoparticles in the flowing stream.

The heat transfer coefficient increased as nanoparticle size increased too. The nanoparticles of 25 nm size have higher value of heat transfer coefficient than the particle size of 50 nm. This is because of the high surface area of SiO₂ nanoparticle to enhance the heat transfer rate of nanofluids.

NOMELECTURE AND GREEKSYMBOLS

Symbol	Description	Units
d	Diameter of the inner tube heat exchanger	m
f	Friction factor	-
h	Heat transfer coefficient	W/ m ² .K
k	Thermal conductivity	W/m.°C
Nu	Nusselt number	$Nu = \frac{hd}{k}$
Pr	Prandtl number	$Pr = \frac{\mu C_p}{k}$
Re	Reynolds number	$Re = \frac{\rho u d}{\mu}$
T	Temperature	°C
u	Fluid velocity	m/s

Units	Description	Symbol
ρ	Density	kg/m ³
μ	Dynamic viscosity	kg/m.s

Symbols	Description
f	Base fluid
nf	Nanofluid
p	Nanoparticle



References

1. SUBRAMANIAN, V. R. K., RAO, N. T., BALAKRISHNAN, A., (editors), Nanofluids and their engineering applications, CRC Press, Taylor and Francis Group, USA, 2020.
2. AHUJA, A.S., Augmentation of heat transport in laminar flow of polystyrene suspensions. I. Experiments and results, *J. Appl. Phys.*, 46, 1975, p. 3408.
3. SUAD, H. D., QUSAY, K. J., ADNAN, M. H., Nanofluid Convective Heat Transfer Enhancement Elliptical Tube inside Circular Tube under Turbulent Flow, *Mathematical and Computational Applications*, 23, 2018, p. 78.
4. SURESHKUMAR, R., THARVES MOHIDEEN, S., NETHAJI, N., Heat transfer characteristics of nanofluids in heat pipes: a review, *Renew. Sust. Energ. Rev.*, 20, 2013, p 397.
5. HLIEVA, OLGA, REABICHIN, S., JELEJNĂI, V., GORDEICIUC, TATIANA, Experimental investigation of the convective heat transfer coefficient of coolants with Al₂O₃ nanoparticle additives, International Conference “Energy of Moldova - 2016. Regional Aspects of development”, 29 September – 01 October 2016, Chişinău, Republica of Moldova.
6. LUCIU, S. R., MATEESCU, TH., COTOROBAI, VICTORIA, MARE, TH., Nusselt number and convection heat transfer coefficient for a coaxial heat exchanger using AL₂O₃ – water pH =5 Nanofluid, *Buletinul Institutului Politehnic din Iaşi*, tom LV (LIX), nr. 2, 2009, p. 71 – 80.
7. MINEA, A.–A., (editor), *Advances in new heat transfer fluids: From numerical to experimental techniques*, CRC Press, Taylor and Francis Group, New York, USA, 2017.
8. CHOI, SUS. Enhancing thermal conductivity of fluids with nanoparticles, *ASME Publications- Fed*, 231, 1995, p. 99.
9. ALFARYJAT, A., STEFANESCU, M.F., DOBROVICESCU, A., Experimental investigation for the thermo-physical properties and stability of CeO₂, ZrO₂, and Al₂O₃ mixed with ethylene glycol and distilled water, *Rev. Chim.*, **70**, (11), 2019, 3908
10. VINAY, SINGH, MUNISH, GUPTA, Heat transfer augmentation in a tube using nanofluids under constant heat flux boundary condition: A review, *Energy Conversion and Management*, 123, 2016, p. 290.
11. PEÑAS, J.R.V., ORTIZ DE Z´ARATE, J.M., KHAYET, M., Measurement of the thermal conductivity of nanofluids by the multicurrent hot-wire method, *J. Appl. Physics*, 104, no.4, Article ID 044314, 2008.
12. NAMBURU, P.K., KULKARNI, D.P., DANDEKAR, A., DAS, D.K., Experimental investigation of viscosity and specific heat of silicon dioxide nanofluids, *Micro and Nano Letters*, 2, no. 3, 2007, p. 67.
13. BOBBO, S., FEDELE, L., BENETTI ET AL., A., Viscosity of water based SWCNH and TiO₂ nanofluids, *Experimental Thermal and Fluid Science*, 36, 2012, p.65.
14. DUANGTHONGSUK, W., WONGWISES, S., An experimental study on the heat transfer performance and pressure drop of TiO₂-water nanofluids flowing under a turbulent flow regime, *International Journal of Heat and Mass Transfer*, 53, 2010, p. 334.
15. VAJJHA, R.S., DAS, D.K., KULKARNI, D.P., Development of new correlations for convective heat transfer and friction factor in turbulent regime for nanofluids *International Journal of Heat and Mass Transfer*, 53, 2010, p. 4607.
16. MINAKOV, A.V., GUZEI, D.V., PRYAZHNIKOV M.I., ZHIGAREV V.A., RUDYAK V.YA., Study of turbulent heat transfer of the nanofluids in a cylindrical channel, *International Journal of Heat and Mass Transfer*, 102, 2016, p. 745.
17. ABDUL HAMID, K., AZMI, W.H., MAMAT, R., SHARMA, K.V., Experimental investigation on heat transfer performance of TiO₂ nanofluids in water–ethylene glycol mixture, *International Communications in Heat and Mass Transfer*, 73, 2016, p. 16.
18. ZARRINGHALAM, M., KARIMIPOUR, A., TOGHRAIE, D., Experimental study of the effect of solid volume fraction and Reynolds number on heat transfer coefficient and pressure drop of CuO–Water Nanofluid, *Experimental Thermal and Fluid Science*, 76, 2016, p. 342.



19. ARMAND, H., GHAREHKHANI, S., SHIRAZI, S.F.S., AMIRI, A., ALEHASHM, M.S., DAHARI, M., KAZI, S.N., Experimental investigation of thermo-physical properties, convective heat transfers and pressure drop of functionalized graphene nanoplatelets aqueous nanofluid in a square heated pipe, *Energy Conversion and Management*, 114, 2016, p. 38.
20. LUCIU, S. R., MATEESCU, TH., Heat transfer study in a coaxial heat exchanger using nanofluids, *Buletinul Institutului Politehnic din Iași, Tom LVI, Fasc. 4*, 2010, p. 73 – 79.
21. AHMET, B.D., MEHMET, D., Prediction of Viscosity Values of Nanofluids at Different pH Values by Alternating Decision Tree and Multilayer Perceptron Methods, *Applied Sciences*, 9, 2019, p. 1288.
22. AZMI, W.H., SHARMA, K.V, SARMA, P.K., RIZALMAN, M., SHAHRANI, A., DHARMA, V., Experimental determination of turbulent forced convection heat transfer and friction factor with SiO₂ nanofluid, *Experimental Thermal and Fluid Science*, 51, 2013, p. 103.
23. DEVDATTA, P., KULKARNI, P., NAMBURU, K., ED BARGAR, H., DEBENDRA, K., Convective Heat Transfer and Fluid Dynamic Characteristics of SiO₂ — Ethylene Glycol/Water Nanofluid, *Heat Transfer Engineering*, 29, no. 12, 2008, p. 1027.
24. HUMINIC, G., Aplicarea nanofluidelor în schimbătoare de căldură, Teză de abilitare, Universitatea Transilvania din Brasov, Brasov, 2015.
25. SUAD, H. D., QUSAY, K. J., ADNAN, M. H., Nanofluid Convective Heat Transfer Enhancement Elliptical Tube inside Circular Tube under Turbulent Flow, *Mathematical and Computational Applications*, 23, 2018, p. 78.
26. VIVEKANAND, L. K., MANIL, R., BHANAVASE, V.L., PATIL, A.J., Effect of Nanoparticle Size on Heat Transfer Intensification, *International Conference on Ideas, Impact and Innova*

Manuscript received: 27.01.2020